



## Thermal Radiation Effects on MHD Casson And Maxwell Nanofluids Over a Porous Stretching Surface

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### ABSTRACT

The main goal of the work is to investigate to the influence the magnetohydrodynamic slip flow through a nonlinear porous stretching surface's upper Maxwell Casson convected nanofluid boundary layer flow was considered. The governing partial differential equations are transformed into nonlinear ordinary differential equations using the proper similarity transformations. The Shooting method was utilized to achieve the numerical solution of the updated equations utilizing the Runge-Kutta-Fehlberg approach. A wide range of essential fluid characteristics were thoroughly examined, including the Schmidt number, magnetic parameter, temperature slip parameter, concentration slip parameter, velocity, and nonlinear stretching parameter. Using graphs and tables, the impacts on temperature, concentration, and velocity were examined and reported. The investigation included calculating and thoroughly debating the skin friction coefficient, local Sherwood numbers, and local Nusselt numbers.

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**Keywords:** Casson Fluid Parameter, Maxwell Fluid, Chemical Reaction Parameter, MHD, Slip Effects.

### 1. Introduction

Potential applications of non-Newtonian fluid flow on porous stretched surfaces include blood flow and engineering. Casson is a liquid that shear thins. It can be a sign of yield stress. When greater yield stress than shear stress is applied, it behaves as a solid; otherwise, it behaves as a liquid and begins to flow. Raju et al<sup>[1]</sup> investigated the Casson fluid application. Gladys et al<sup>[2]</sup> Contributions of variable viscosity and thermal conductivity on the dynamics of non-Newtonian nanofluids flow past an accelerating vertical plate. Reddy et al<sup>[3]</sup> are examined the effect of radiation on MHD mixed convection oscillatory flow over a vertical surface in a porous medium with chemical reaction and thermal radiation. Sandhya et al<sup>[4]</sup> have analysed the heat and mass transfer effects on MHD flow past an inclined porous plate in the presence of chemical reaction. For the magnetohydrodynamic Carreau and Casson fluids, Kumaran et al.<sup>[5]</sup> have studied the exponential heat source/sink, momentum,

and thermal transport over the spinning paraboloid. A study on free convective heat and mass transfer flow through a highly porous medium with radiation, chemical reaction and Soret effect is analysed by Suneetha et al<sup>[6]</sup>. Sobamowo et al<sup>[6]</sup>. have looked at the effects of additional control features on the stream and heat transfer qualities to the nanofluids when the base fluid is implanted with the upper and silver nanoparticles.

Unsteady Carreau-Casson fluids in a solution of dust and graphene nanoparticles with non-Fourier heat flux across a radiating shrinking layer have been explored by Santosh et al.<sup>[7]</sup>. Santosh et al.<sup>[8]</sup> have studied the computational examination of 3D Casson-Carreau nanofluid flow. A colloidal postponement called nano fluid contains nanoparticles in a base fluid. Nano fluids have a wide range of uses in engineering, from the automotive industry to the medical sector. They are used in nuclear reactors, power plant cooling systems, geothermal energy extraction, automotive applications, electronic applications like cooling microchips, and biomedical applications like cancer therapeutics and nano cryosurgery, among other things. Due to these real characteristics, nano fluids are significant to investigate, as shown by the references<sup>[9-14]</sup> in this debate. The

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non-Newtonian fluid flow across a mixed stretchable surface has been studied with different variables by Chandra and Sandeep<sup>[15]</sup>, Reddy et al.<sup>[16]</sup>, and Tian et al.<sup>[17]</sup>. Nasir et al.<sup>[18]</sup> looked at how thermal radiation affected MHD 3D flow across a stretched surface. A nano liquid film's Eyring-Powell slip flow has been studied by Khan et al.<sup>[19]</sup>.

In-depth references<sup>[20-26]</sup> on this topic examined non-Newtonian Maxwell fluids under a range of physical circumstances, including viscous dissipation, Newtonian heating, homogeneous-heterogeneous chemical interactions, and thermal stratification over a variety of stretching surfaces. They found that when the Prandtl number climbed, both temperature and heat transfer rate dropped. The effect of radiation and convective boundary limitation on the oblique stagnation point of the non-Newtonian nano fluids past the stretching layer was studied by Abuzar et al.<sup>[24]</sup>. Yasin et al numerical study of the stagnation point flow of nano fluid considers the sloped stretched sheet.

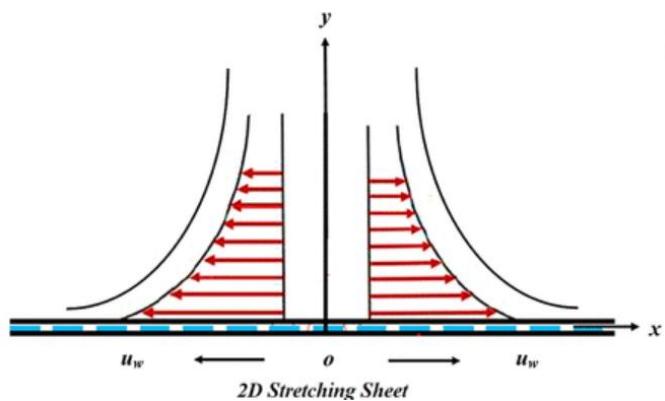
The effects of slip on MHD flow have been studied by certain researchers<sup>[25-27]</sup> using a variety of non-Newtonian nano fluid models, such as Casson fluid and Jeffery nano-fluid, across a flexible sheet with varied physical limits. Ibrahim et al.<sup>[28]</sup> investigation of the influence of chemical reaction on mass and heat transport characteristics. Nevertheless, the sources addressing chemical reactions and slip effects are addressed in references<sup>[29-48]</sup>.

The analysis of the MHD stagnation point flow of upper-convected Maxwell fluid with chemical reaction is not considered by any of the researchers due to the impacts of nanoparticles with slip effects. Therefore, using the Runge-Kutta Fehlberg method and the shooting technique, the current paper aims to investigate the impact of nanoparticle and chemical reaction on MHD slip stagnation point flow, boundary layer flow, and heat and mass transfer of upper-convected Casson and Maxwell fluid above a stretching sheet. This work is unusual because it incorporates the influence of nanoparticles with chemical reaction and slip effect in upper-convected MHD Casson and Maxwell fluids.

## 2. Mathematical Formulation

Consider the 2D motion of a non-Newtonian nano fluid with time dependence and incompressibility, as well as heat radiation and chemical reaction over a porous stretched surface under convective circumstances. The Free stream velocity  $u_f(x)$  and the stretching velocity  $u_w(x)$  are of the forms  $u_f(x) = ax$  and  $u_w(x) = bx$  where  $a$  and  $b$  are constants. The  $x$ -axis is along the sheet and normal to the sheet  $y$ -axis is chosen. The concentration is represented by  $C_w$  and the temperature is represented by  $T_w$  and the ambient concentration and ambient temperature are represented by  $C_\infty$  and  $T_\infty$ .

The physical model of the flow and Cartesian coordinates are shown in Fig. 1. The proposed Casson model for two-dimensional laminar steady flow has governing differential equations that are expressed in the following form:



**Figure 1:** Physical model of the problem.

The flow expressions are defined as<sup>[34]</sup>

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \quad (1)$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \left[ \left( 1 + \frac{1}{\gamma} \right) v \frac{\partial^2 u}{\partial y^2} - \zeta \left( u^2 \frac{\partial^2 u}{\partial x^2} + v^2 \frac{\partial^2 u}{\partial y^2} + 2uv \frac{\partial^2 u}{\partial x \partial y} \right) + u_f \frac{\partial u_f}{\partial x} - \left( \frac{\sigma B_0^2}{\rho_f} + \frac{v}{K_1} \right) (u_l - u) \right] \quad (2)$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha \frac{\partial^2 T}{\partial y^2} + \tau \left( D_B \frac{\partial C}{\partial y} \frac{\partial T}{\partial y} + \frac{D_T}{T_\infty} \left( \frac{\partial T}{\partial y} \right)^2 \right) - \frac{1}{(\rho c_p)_f} \frac{\partial q_r}{\partial y} + \frac{Q_0(T - T_\infty)}{(\rho c_p)_f} \quad (3)$$

$$u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} = D_B \frac{\partial^2 C}{\partial y^2} + \frac{D_r}{T_\infty} \frac{\partial^2 T}{\partial y^2} - K_r (C - C_\infty) \quad (4)$$

The Navier slip conditions, convective conditions and Nield boundary conditions are assumed as follows:

$$u = ax + m_1 \frac{\partial u}{\partial y}, v = 0, T = T_w + m_2 \frac{\partial T}{\partial y}, \\ C = C_w + m_3 \frac{\partial C}{\partial y} \text{ at } y = 0 \\ u \rightarrow u_e(x) = bx, v \rightarrow 0, T \rightarrow T_\infty, C \rightarrow C_\infty \text{ as } y \rightarrow \infty \quad (5)$$

where  $u$  and  $v$  are the velocity components along the  $x$  and  $y$  directions,  $\rho_f$  is the density of the base fluid,  $\alpha$  – is the thermal diffusivity,  $\zeta$  is the relaxation time parameter of the fluid,  $B_0$  is the strength of the magnetic field,  $v$  is the kinematic viscosity of the fluid,  $K_1$  is the permeability parameter,  $\gamma$  is the Casson fluid parameter,  $D_B$  is the Brownian diffusion coefficient,  $D_r$  is the thermophoretic diffusion coefficient,  $\tau$  is the ratio between the effective heat capacity of the nano particle material and heat capacity of the fluid,  $C$  is the volumetric volume expansion coefficient, and  $\rho$  is the density of the particle,  $K_r$  is the chemical reaction rate,  $m_1, m_2$ , and  $m_3$  are the velocity slip, thermal slip and concentration slip conditions respectively..

The radiation heat flux ( $q_r$ ) is modeled by using Rosseland approximation given in:

$$q_r = - \left( \frac{4\sigma^*}{3k_1} \right) \frac{\partial T^4}{\partial y} \quad (5)$$

Here  $\sigma^*$  represents the constant of Stefan-Boltzmann,  $k_1$  gives the coefficient of mean absorption. It is also assumed that if the difference in temperature within the flow is  $T^4$ , then  $T^4$  can be expressed as a linear combination of the temperature by expanding the  $T^4$  by Taylor's series about  $T_\infty$  to obtain (7):

$$T^4 = T_\infty^4 + 4T_\infty^3(T - T_\infty) + 5T_\infty^2(T - T_\infty)^2 + \dots \quad (7)$$

If we neglect the higher order beyond the first degree in  $(T - T_\infty)$  in this series and opening brackets on the right-hand sides of (7) we obtain (8):

$$T^4 \approx -3T_\infty^4 + 4T_\infty^3T \quad (8)$$

Substituting the right-hand side of (8) into (5) for  $T^4$  yield (9):

$$\begin{aligned} q_r &= -\left(\frac{4\sigma^*}{3k_1}\right)\frac{\partial T^4}{\partial y} = -\left(\frac{4\sigma^*}{3k_1}\right)\frac{\partial}{\partial y}(-3T_\infty^4 + 4T_\infty^3T) = \\ &= -\left(\frac{15T_\infty^3\sigma^*}{3k_1}\right)\frac{\partial T}{\partial y} \end{aligned} \quad (9)$$

The rate of change in radiative heat flux with respect to  $y$  is given by (13)

$$\frac{\partial q_r}{\partial y} = -\left(\frac{16T_\infty^3\sigma^*}{3k_1}\right)\frac{\partial^2 T}{\partial y^2} \quad (10)$$

The partial differential equations (2),(3),(4) and (5) are transformed into ordinary differential equations by introducing the dimensionless variables are given by (11):

$$\psi = \sqrt{cv}f(\eta), \theta(\eta) = \frac{(T-T_\infty)}{(T_w-T_\infty)}, \phi(\eta) = \frac{(c-c_\infty)}{(c_w-c_\infty)}, \eta = \sqrt{\frac{c}{v}}y \quad (11)$$

The stream function velocity  $\psi$  can be defined as  $u = \frac{\partial \psi}{\partial y}, v = -\frac{\partial \psi}{\partial x}$  so that equation (1) satisfies the continuity equation.  $f(\eta)$  denote the injection and suction,  $\eta$  is the dimensionless space variable,  $\theta(\eta)$  and  $\phi(\eta)$  are the dimensionless of temperature and concentration of the fluid respectively.

In view of the above-mentioned transformations equations (2), (3) and (48) are reduced to the following ODEs:

$$\begin{aligned} \left(1 + \frac{1}{\gamma}\right)f''' + ff'' - f'^2 + E^2 + (M + 1/K)(E - f') + \\ \delta(2ff'f'' - f''') = 0 \end{aligned} \quad (12)$$

$$\begin{aligned} \left(1 + \frac{4}{3R}\right)\theta'' + Pr f \theta' + Pr N b\phi'\theta' + Nt\theta'^2 + Pr Q \theta = 0 \\ (13) \end{aligned}$$

$$\phi'' + Le\phi' + \frac{Nt}{Nb}\theta'' - KrLe\phi = 0 \quad (14)$$

The transformed boundary restrictions are:

$$\begin{aligned} f(\eta) &= S, f'(\eta) = 1 + L_1f''(\eta), \theta(\eta) = 1 + L_2\theta'(\eta), \phi(\eta) \\ &= 1 + L_3\phi'(\eta) \text{ at } \eta = 0 \\ f'(\eta) &\rightarrow E, \theta(\eta) \rightarrow 0, \phi(\eta) \rightarrow 0 \text{ as } \eta \rightarrow \infty \end{aligned} \quad (15)$$

where  $f'$  is dimensionless velocity,  $\theta$  is dimensionless temperature,  $\phi$  is dimensionless concentration, and  $\eta$  is the

similarity variable. The prime denotes differentiation with respect to  $\eta$ .

The skin friction  $C_f$ , local Nusselt number  $Nu_x$  and Sherwood number  $Sh_x$  are the important physical quantities they can be defined as follows<sup>[34]</sup>:

$$C_f = \frac{\tau_w}{\rho u_w^2}, Nu_x = \frac{xq_w}{k(T_f - T_\infty)}, Sh_x = \frac{xq_m}{D_B(c_w - c_\infty)}$$

Here  $\tau_w = \mu(1 + \beta)\frac{\partial u}{\partial y}$  is the surface shear stress,  $q_w = -k\left(\frac{\partial T}{\partial y}\right)_{y=0} + q_r$  is the surface heat flux and  $q_m = -D_B\left(\frac{\partial c}{\partial y}\right)_{y=0}$

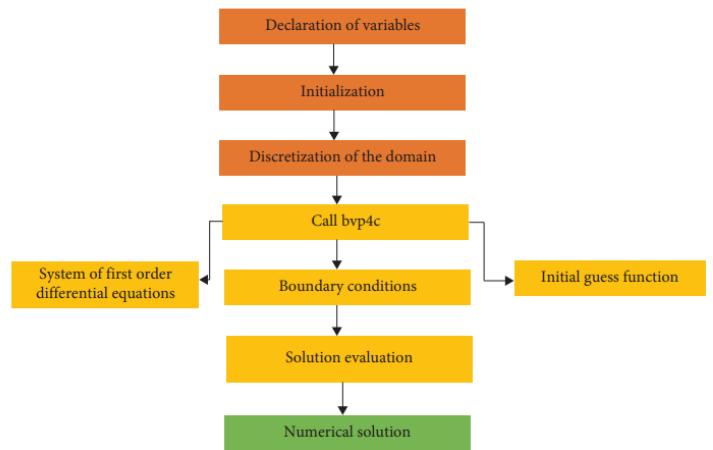
Using the similarity transformation in (11) we have the following relations:

$$C_f Re_x^{\frac{1}{2}} = f'(0), Nu_x Re_x^{-\frac{1}{2}} = -\left(1 + \frac{4}{3R}\right)\theta'(0), Sh_x Re_x^{-\frac{1}{2}} = -\phi'(0)$$

where  $Re_x$  is the local Reynolds number.

### 3. Numerical Solution

The fourth order Runge-Kutta Fehlberg method based on the shooting scheme is used to solve the system of nonlinear coupled ordinary differential equations (12-14) subject to the boundary constraints (15). This study emphasizes the characteristics of motion, heat, and mass transmission. The field of velocity, energy, and concentration profile, as well as friction factor, Nusselt number, and Sherwood number, are all properly investigated.



Flow chart of Numerical scheme (BVP4C)

$$\begin{aligned} f &= f(1), f' = f(2); f'' = f(3); \theta = f(4); \theta' = f(5); \phi \\ &= f(6); \phi' = f(7); \\ f'(3) &= f(1)f(3) - f(2)^2 + E^2 + (M + 1/K)(E - f(2)) \\ &+ \delta(2f(1)f(2)f(3))/(1 + 1/\gamma + \delta) \\ f'(5) &= -(Pr f(1)f(5) + Pr N b f(7)f(5) + Nt f(5)^2 \\ &+ Pr Q f(4))/(1 + (4/3)R) \end{aligned}$$

$$\begin{aligned}
f'(7) = & -Lef(7) \\
& + \frac{Nt}{Nb} \left( (Pr f(1)f(5) + Pr N bf(7)f(5) \right. \\
& \left. + Ntf(5)^2 + Pr Q f(4)) / (1 + (4/3)R) \right) \\
& - KrLef(6)
\end{aligned}$$

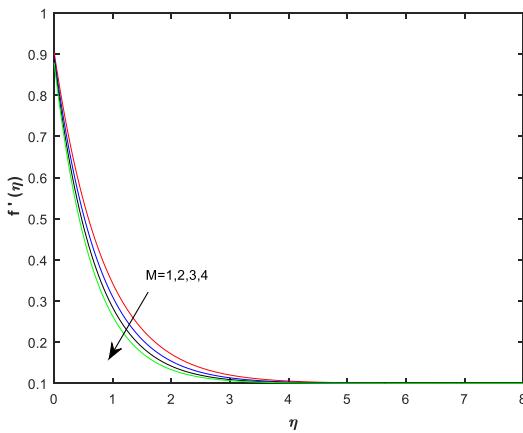
#### 4. Results and Discussion

In this connection the successive outcomes for physical variables are evaluated  $M=0.5$ ,  $\beta=0.1$ ,  $\gamma=0.2$ ,  $Pr=0.71$ ,  $Le=1.0$ ,  $Nb=0.1$ ,  $S=0.5$ ,  $Nt=0.1$ ,  $R=0.2$ ,  $Kr=0.2$ ,  $Q=0.1$ ,  $E=0.01$ . For this study, the successive outcomes for physical variables are evaluated.

Figure 2 depicts how the magnetic field's properties affect the flow velocity. It has been shown that the magnetic parameter generates the Lorentz force, which causes the fluid's velocity to slow down and the velocity profile to rise to higher magnetic parameter values. Figure 3 shows the variation of velocity profiles for various permeability parameter values (K). It is evident that the presence of a porous media increases the fluid flow's values, which accelerates the fluid. As a result, the influence of increasing permeability parameter values on fluid velocity results in a thickening of the thermal boundary layer.

The fluid's velocity is decreased by the Casson effect in Figure 4. It is crucial because the yield stress of the Casson fluid is lowering. Physically, a decrease in the yield strain appears to be caused by an increase in the Casson parameter, which raises the liquid's plastic dynamic viscosity and thickens the momentum boundary layer.

The temperature curves for various estimates of the thermal radiation parameter are shown in Figure 5. When thermal radiation calculations are improved, it is discovered that the temperature profile and the thickness of the temperature boundary layer rise. When the estimates of  $Pr$  were improved and the thermal diffusivity was decreased, the temperature and



**Figure 2:** Velocity Profile for various values of M

thermal boundary layer thickness fell, which led to a decrease in the temperature profile, as shown in Figure 6. The relative thickness of momentum and thermal boundary layers is governed by how quickly and slowly heat diffuses depending on  $Pr$ .

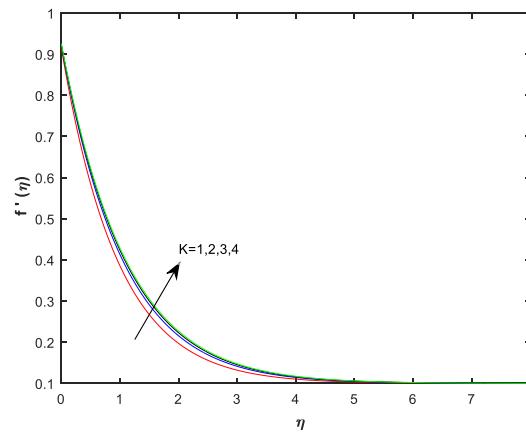
Figure 7 shows how temperature profiles with increasing  $Q$  values improve the thermal boundary layers. When a heat source is present, the energy is delivered to the flow. The energy enhances the thermal boundary layers. The concentration in this figure drops as the thermophoresis parameter values rise.

Figure 8 illustrates how the thermophoresis parameter affects the concentration profiles. As  $Nt$  rises, the thermal and concentration boundary layers get thicker. As the temperature and  $Nb$  temperature curves in Figure 9. At the surface, the thermal boundary layer's thickness is seen to be increasing.

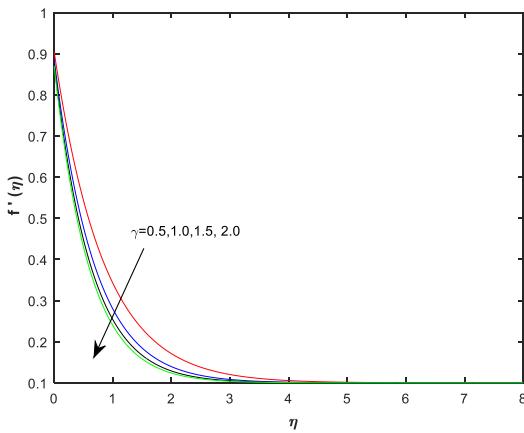
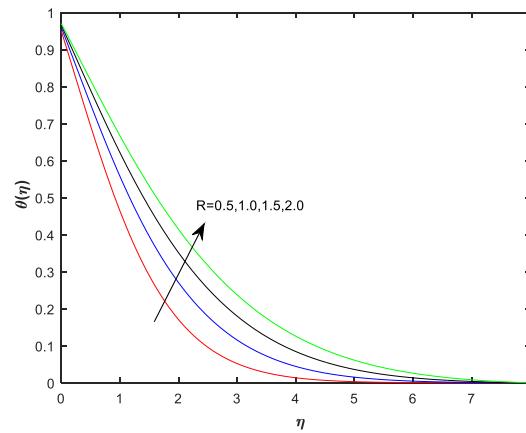
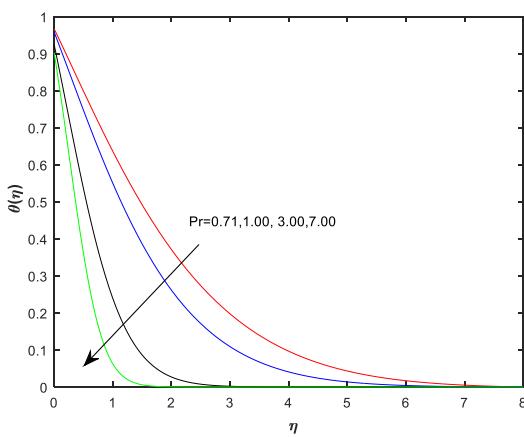
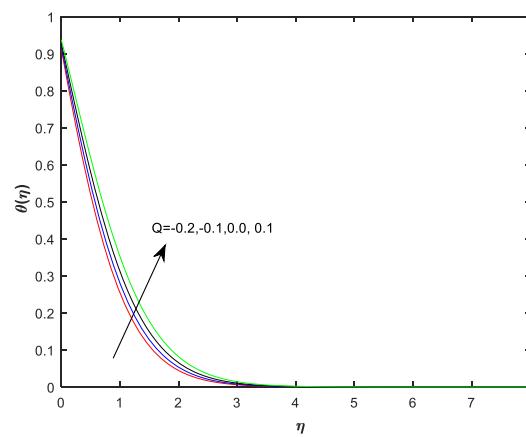
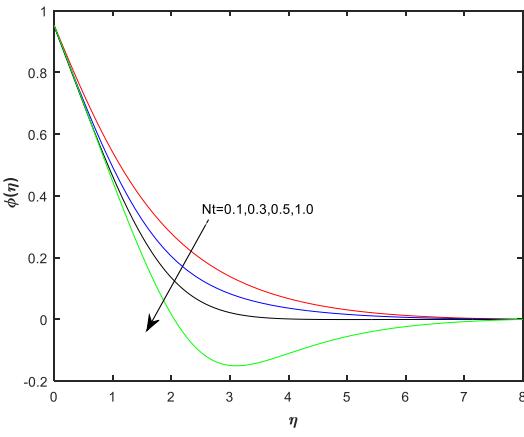
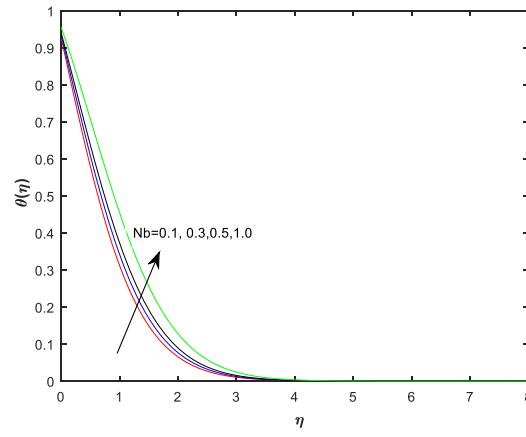
The concentration profile for various  $Kr$  levels is shown in Figure 10. It was observed that the concentration profile decreased with an update to the  $Kr$ . This demonstrates how thickening the concentration boundary layer results in a drop in the concentration profile due to an increase in the chemical reaction parameter.

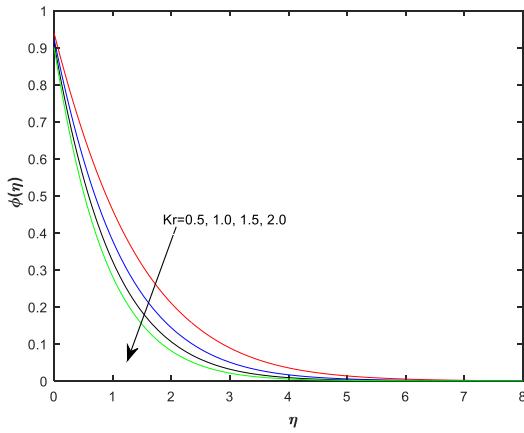
The effect of the Lewis number on concentration profiles is seen in Figure 11. The graphic shows that the thickness of the concentration graph and the concentration border layer decreases with increasing Lewis number values.

For different values of  $B, Q, Nt, Nb, Kr, Le, L_1, L_2, L_3$  and  $S$ , the variation of  $-f''(0)$ ,  $-\theta'(0)$  and  $-\phi'(0)$  is given in Table 1. The table shows that when the suction-injection parameter  $S$  and Deborah number grow, the skin friction coefficient rises but falls with an increase in the velocity ratio  $E$  and the velocity slip parameter. The table also demonstrates how the local Nusselt number and the local Sherwood number of the flow region change when the values of  $S$  and  $E$  change in response to changes in Deborah number and velocity slip parameter  $L_1$ .

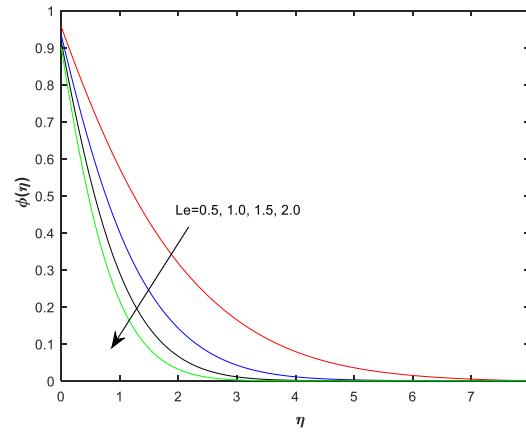


**Figure 3:** Velocity Profiles for various values of K.

**Figure 4:** Velocity Profile for various values of  $\gamma$ **Figure 5:** Temperature Profile for various values of  $R$ .**Figure 6:** Temperature Profile for various values of  $Pr$ .**Figure 7:** Temperature Profile for various values of  $Q$ .**Figure 8:** concentration Profile for various values of  $Nt$ .**Figure 9:** Temperature Profile for various values of  $Nb$ .



**Figure 10:** Concentration Profile for various values of Kr



**Figure 11:** Concentration Profile for various values of Le

**Table 1:** The estimates of skin friction factor, Nusselt number, Sherwood number for different values of B,Q,Nt,Nb,Kr,Le,L<sub>1</sub>,L<sub>2</sub>,L<sub>3</sub> and S.

B	Q	Nt	Nb	Kr	Le	L <sub>1</sub>	L <sub>2</sub>	L <sub>3</sub>	S	-f''(0)	-θ'(0)	-ϕ'(0)
0.5	0.1	0.1	0.1	0.1	0.1	0.1	0.1	0.1	0.1	0.953373	0.544371	0.755949
1										1.141595	0.557514	0.770805
1.5										1.235429	0.579709	0.795489
2										1.294181	0.524531	0.845122
0.1	-0.2	0.1	0.1	0.1	0.1	0.1	0.1	0.1	0.1	0.957215	0.523708	0.844095
	-0.1									0.957215	0.717854	0.928702
	0									0.957215	0.799153	1.002185
	0.1									0.957215	0.871248	1.057552
0.1	0	0.1	1	0.1	0.1	0.1	0.1	0.1	0.1	0.957215	0.190038	0.452225
		0.3								0.957215	0.287873	0.479390
		0.5								0.957215	0.352388	0.488595
		1								0.957215	0.439895	0.495879
0.1	0	0.1	0.1	0.1	0.1	0.1	0.1	0.1	0.1	0.957215	0.439895	0.452225
		0.3								0.957215	0.585888	0.512357
		0.5								0.957215	0.550337	0.581223
		1								0.957215	0.717854	0.928702
0.2	0	0.1	11	0.5	0.1	0.1	0.1	0.1	0.1	0.957215	0.000001	0.514295
				1						0.957215	0.000001	0.759525
				1.5						0.957215	0.000001	0.891445
				2						0.957215	0.000002	0.993955
0.2	0	0.1	11	0.1	0.5	0.1	0.1	0.1	0.1	0.957215	0.000000	0.437074
					1					0.957215	0.000000	0.553544
					1.5					0.957215	0.000001	0.842443
					2					0.957215	0.000004	0.993947
0.2	0	0.1	11	0.1	0.5	0.5	0.1	0.1	0.1	0.309825	0.000001	0.351835
						1				0.375415	0.000002	0.351417
						1.5				0.477157	0.000002	0.375832
0.2	0	0.1	11	0.1	0.5	0.5	0	0.1	0.1	0.558051	0.000003	0.400170
							0.5			0.957215	0.000002	0.270932
							1			0.957215	0.000042	0.313497
							1.5			0.957215	0.000308	0.371921
0.2	0	0.1	11	0.1	0.5	0.5	0.1	0	0.1	0.957215	0.001245	0.457090
								0.5		0.957215	0.000042	0.313497
								1		0.957215	0.000308	0.371921

0.2	0	0.1	11	0.1	0.5	0.5	0.1	1.5	0.957215	0.001245	0.457090
								0	0.942580	0.000003	0.407555
								0.5	1.020500	0.000012	0.551738
								1	1.113429	0.000033	0.728104
								1.5	1.225358	0.000071	0.899954

## 5. Conclusion

This study uses a chemical reaction on a stretchable sheet to explain the MHD slip effect and Casson upper convected Maxwell fluid stagnation point flow. The governing parameters, such as the velocity ratio, suction-injection parameter, Lewis numbers, Deborah number, magnetic field, Brownian motion parameter, thermophoresis parameter, chemical reactions parameter, thermal radiation parameter, velocity slip parameter, thermal slip parameter, singular slip parameter, Casson fluid parameter, and heat source parameter. The information about this paper is shown as follows:

- The effect of the magnetic field parameter's increase on the velocity field is lessened.
- The velocity field increases with rising magnetic field, while it decreases with rising solutal slip values.
- Concentration profiles are decreased by enhancing the values of Brownian motion, chemical reaction, Lewis number, thermal slip parameter, and singular slip parameter.
- The characteristics of velocity profiles with regard to changes in the suction parameter lead to a weakening of the velocity field.

## Conflict of interests

None

## Author Contribution

The authors contributed equally to this work, from the implementation and design of the research, the analysis of the results and to the writing of the manuscript.

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